



Gilbertson, M. A., Taylor, A., Mitchell, S., & Rust, A. C. (2020). A fluidisation mechanism for secondary hydroeruptions in pyroclastic flow deposits. *Frontiers in Earth Science*.
<https://doi.org/10.3389/feart.2020.00324>

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A Fluidisation Mechanism for Secondary Hydroeruptions in Pyroclastic Flow Deposits

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OPEN ACCESS

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Specialty section:

This article was submitted to
Volcanology,
a section of the journal
Frontiers in Earth Science

Received: 16 March 2020

Accepted: 13 July 2020

Published: 02 September 2020

Citation:

Gilbertson MA, Taylor A, Mitchell SJ
and Rust AC (2020) A Fluidisation
Mechanism for Secondary
Hydroeruptions in Pyroclastic Flow
Deposits. *Front. Earth Sci.* 8:324.
doi: 10.3389/feart.2020.00324

Heating of water under hot pyroclastic flow deposits can drive hydroeruptions, forming craters and aprons of secondary deposits. According to the established conceptual model, steam pressure builds until failure of the pyroclastic overburden and a relatively low permeability (fine-grained) cap promotes secondary explosions. We explore a complementary model where the stress from drag related to gas flow up through the particle interstices is comparable in magnitude to the static pressure difference between the base and the top of the pyroclastic flow deposit. The drag force supports (part of) the weight of the particles and so reduces inter-particle friction; in a mono-sized bed this friction is effectively eliminated at the “minimum fluidisation velocity,” which depends on the size and density of the particles. Through analogue experiments we show that violent outbursts can be generated when there are vertical variations in the minimum fluidisation velocities of granular materials. We ran experiments with layers of particles with different sizes or size distributions (bi-modal with different proportions of fine and coarse particles) in a tank with a porous base that allowed a distributed upward airflow through them. A finer-grained layer capping a coarser layer does not generate jets of particles or craters; rather, increased gas flux leads to fluidisation of first the fine and then the coarse (lower) layer. However, when the upper layer is coarser, the bed domes upward as a gas pocket grows within the finer layer for some combinations of layer thicknesses and grain sizes. When the gas pocket penetrates the top of the bed, it forms a crater and erupts particles. The gas velocity when doming initiates is greater than that calculated for the weight of the top layer to be balanced by drag and the pressure difference across that layer. This discrepancy is explained by the layers having a strength (from inter-particle friction), which is consistent with the observed dependence of the initiation velocity on the absolute thickness of the layer. Using data from Mt St Helens 1980 deposits, we show that the drag-related trigger observed in the laboratory is a feasible mechanism for secondary hydroeruptions through pyroclastic flow deposits.

Keywords: fluidisation, pyroclastic flow, secondary eruption, hydroeruption, drag, granular, jet, minimum fluidisation velocity

1. INTRODUCTION

Pyroclastic flows are currents of hot particles and gases which travel down valleys and spread laterally under gravity, and so are often deposited in stream-valleys and near-shore environments. Steam generated by heating surface water or shallow groundwater under a pyroclastic deposit may escape passively via fumaroles or diffusively through the permeable deposit; however, under some conditions the steam can drive sudden secondary eruption(s) through the primary pyroclastic flow deposit leaving craters, surge deposits and fallout from ballistics and tephra fountaining (e.g., Moyer and Swanson, 1987; Keating, 2005).

The secondary eruption craters spatially associated with water sources in historic pyroclastic flow deposits including those of Mount St Helens 1980 (e.g., Moyer and Swanson, 1987), Redoubt 1990 (Gardner et al., 1994), Mount Pinatubo 1991 (Torres et al., 1996) and Katmai (Valley of Ten Thousand Smokes) 1912 (e.g., Hildreth, 1983), suggest that it is common to form secondary hydroeruptions when hot pyroclastic flows are deposited on a wet terrestrial environment. Not only are they a hazard to people near freshly emplaced pyroclastic flows, they are a potential trigger for destabilisation and remobilisation of pyroclastic material, forming secondary flows with more distal effects: the secondary ignimbrites after the main 1991 eruption of Mount Pinatubo travelled up to 10 km and generated ash clouds up to 10 km high (Torres et al., 1996). Their common occurrence and associated hazards motivate a better understanding of mechanisms for generating secondary explosive hydroeruptions in pyroclastic flow deposits. There are likely to be multiple mechanisms; here we only consider the scenario of a non-welded pyroclastic flow deposit with an underlying water source and not any mechanisms that involve welding nor cohesion nor water gulleying down into hot pyroclastic material (e.g., Torres et al., 1996).

When a fluid (e.g., steam) source is set under a layer of granular material then fluid will flow through the layer at a rate determined by the permeability of the layer and the pressure gradient across it. If the layer is not sufficiently permeable for the flow through it to match the rate of fluid generated at the source, then the source pressure will increase until fluid leaves the source at the same rate as it is generated. The forces exerted on the granular layer by the fluid are due to both the pressure difference generated across it, which pushes up on the base of the layer, and the drag caused by the flow through it, which pushes up on particles throughout the thickness of the layer (van der Hoef et al., 2005). These forces are opposed by the weight of the granular layer and the inter-particle friction within it. When these forces are exceeded by those generated by the source, then the layer will fail.

The modelling of secondary hydroeruptions has concentrated on the build-up of pressure. Moyer and Swanson (1987) proposed what we term a “static pressure build-up” model for secondary hydroeruptions in pyroclastic flow deposits (also discussed by Keating, 2005), building on their and other’s (Rowley et al., 1981) observations from Mount St Helens 1980–1981. This remains the best-documented and most-studied set of secondary hydroeruptions. Most of the secondary craters formed within a few days of the emplacement of the May 18, and to a lesser

degree the June 12 1980, pyroclastic flows that were deposited on top of May 18 debris avalanche material; however, there were some secondary eruptions much later, including one in May 1981 that was filmed (Moyer and Swanson, 1987). Photographs of craters dotting the landscape and a vertical section through a crater later exposed by fluvial erosion are found in Rowley et al. (1981) and Brand et al. (2014) respectively. The craters were generally near-circular in plan, 5–100 m diameter and 1–20 m deep. There is a clear spatial association of the craters with pre-1980 stream-valleys even though the streams were disrupted by the debris avalanche. Moyer and Swanson (1987) inferred that the source of steam driving the secondary eruptions was water ponded on the debris avalanche deposit at the base of the pyroclastic flows and not deeper groundwater because the secondary eruption products are lacking in clasts of the distinctive May 18 “blast dacite” (cryptodome) from the debris avalanche under the primary pyroclastic flow deposits.

The “static pressure build-up” model (Moyer and Swanson, 1987; Keating, 2005) involves steam generation at the base of the hot pyroclastic flow deposit at a rate faster than it escapes, until the steam pressure reaches some critical value slightly exceeding lithostatic pressure (Keating, 2005), causing failure of the deposit. This failure causes rapid rise of steam, including steam flashed from water that became superheated due to the sudden decompression when the pyroclastic overburden failed. Thus factors that should control explosive vs. passive steam release include the rate of steam generation (i.e., availability of water and rate of heat transfer) and the deposit permeability, which if not welded depends on the grain size distribution and packing. Moyer and Swanson (1987) emphasise the importance of the permeability of the pyroclastic overburden in regulating the eruptive phenomena, with finer-grained, lower permeability deposits more conducive to explosive steam release; Torres et al. (1996) even suggest that a confining layer of fine ashfall can significantly inhibit the release of pore pressure in pyroclastic flow deposits. Torres et al. (1996) note that increased pore pressure within the pyroclastic flow deposit would decrease its strength, and Moyer and Swanson (1987) discuss the possibility that increased pore pressure might expand (de-compact) the pyroclastic material and so increase its permeability (with potential complex feedback if localised). However, there is no consideration of the dynamic drag force pushing up on pyroclasts throughout the deposit that is related to gas flow up through the pore space between the particles.

In this paper we explore an alternative mechanism for secondary hydroeruptions where the drag force is critical, and variations in grain size distribution of the pyroclastic flow deposit matter not because grain size affects permeability but because it affects the gas flux at which the drag force supports the weight of the particles. Using analogue experiments we show how it is possible for violent eruptions to take place in layered beds where the top layer is more permeable than the bottom when gas is passed through them. We argue that the observed behaviour is a result of the interaction between the particles and the fluid, the flow pattern induced in the bed of particles, and the collective mechanical properties of the particles. The mechanism we propose for secondary hydroeruptions has many similarities

(and some differences) with that proposed by Nichols et al. (1994) to explain fluid escape structures in layered sediments in areas of rapid sedimentation in water. For both applications, it is important to understand the role of internal friction in the deformation and fluidisation of granular materials.

A granular layer can deform in response to a stress applied at a margin (e.g., pushing up on the base of the layer) because the particles transmit force to each other through friction, enabling them to behave collectively; however, it can also deform when there is a vertical fluid flow through the interstices of the granular layer owing to the drag exerted. In a bed with fluid flow up through the particles, the weight of the particles will be opposed by the drag, and so friction between particles decreases. If the particles are monosized and the flow rate is large enough to support the entire weight of the bed (the “minimum fluidisation velocity,” u_{mf}) then friction between the particles will be eliminated and the layer does not deform collectively. For a simple bed of uniform particles, u_{mf} is greater (i.e., a greater fluid velocity is needed to support the weight of the particles) for larger and/or denser particles (e.g., Rhodes, 1998).

Nichols et al. (1994) suggested that fluidisation might be an important process for the violent breaching of a layer of particles subject to a fluid flow through them. In their laboratory experiments they observed water flow up through water-saturated layered beds in which a layer of larger (or denser) particles overlaid a layer of smaller (or less dense) particles in a tank with a solid porous base to provide a distributed water source. At water velocities greater than u_{mf} of the bottom layer but less than u_{mf} of the top layer, the bottom layer divided so that a void (i.e., a pocket of water) formed between a fluidised layer of small particles at the bottom of the tank and a static layer of small particles pressed up against the base of the layer of large particles above it. In this condition, the drag exerted on the static layer of small particles exceeded that necessary to support its weight, and so this excess drag allowed these small particles to support the layer of larger particles. If the fluid velocity was increased so that the total drag on the top, composite (coarse and fine) layer exceeded its weight, the composite layer deformed until it suddenly failed, releasing a plume of particles into the water above it. Unlike secondary hydroeruptions in pyroclastic deposits, the burst-out and jetting in these experiments did not generate conical craters in the top of the granular bed.

We present new experiments that, like those of Nichols et al. (1994), involve fluid flow up through layers of particles in a tank with a porous base. However, a key difference is that the fluid is gas (air) rather than liquid water. The associated difference in buoyancy and Reynolds number will affect inter-particle forces and drag, and so the mechanical response of the layers and the fluidisation dynamics. For example, it is well-established in chemical engineering that in gas-fluidised systems, when the gas velocity exceeds u_{mf} , the excess gas flow forms bubbles that rise through the bed, whereas in liquid-fluidised beds, bubbles do not form and the bed expands when the velocity exceeds u_{mf} (Davidson and Harrison, 1963). These differences make the new experiments more relevant to secondary hydroeruptions in pyroclastic deposits.

We have kept the experiments simple in order to identify the key physical processes involved and to isolate the effects of individual factors. The goal is to test whether a fluidisation mechanism for triggering secondary hydroeruptions is feasible and not to reproduce the full dynamics of the eruptions. For example we use room-temperature air and a bed thickness of order 10 cm rather than steam and a deposit thickness of tens of metres, which means the analogue eruptions are not boosted by sudden decompression-induced flashing of superheated water to steam as in nature. A more fundamental simplification is representing the primary pyroclastic flow deposit as layers of uniform-density spheres with narrow unimodal or bimodal size distributions. Pyroclastic flow deposits often have complex vertical and lateral facies changes and broad particle size distributions from ash to blocks, and a range of clast densities from lithics to pumice. However, due to multiple flow units and pulses, as well as changes in conditions with time as the deposit is progressively aggregated, there can be sub-horizontal layers defined by changes in grain size distribution and componentry (e.g., dense lithic content) on the scale of interest to this study (e.g., tens of metres). Such layering is present in the pyroclastic flow deposits of Mount St. Helens 1980, as shown in the photographs and data from vertical sections exposed by fluvial incision presented in Brand et al. (2014). In a fluidisation mechanism for secondary hydroeruption triggering, we hypothesise that what matters is vertical variations in u_{mf} , not whether the size (or density) distribution of particles is narrow or broad. We make use of a huge body of work on fluidised beds, mostly in chemical engineering (but also in volcanology), with particles of different size, density, shape, and packing in order to relate the results of our simplified experiments to more complicated natural conditions.

2. EXPERIMENTAL METHODS AND MATERIALS

The experiments were conducted with beds of particles in a transparent Perspex, vertical, planar (near-2D) container with a rectangular cross-section 300 mm by 8 mm as shown in **Figure 1**. The base was fitted with a porous plastic distributor (Vyon “D,” pore size nominally 20 μm) to ensure uniform gas distribution into the base of the bed of particles, which was fluidised using air from a central supply, controlled and metered by rotameters to a maximum accuracy of 2 mm/s for superficial gas speed in the particle bed. The upstream pressure was set by a pressure regulating valve at 1 bar. The particles were glass spheres (ballotini) with density $\rho_p = 2,500 \text{ kg/m}^3$, chosen for their known and uniform properties.

The ballotini were sieved and the nominal diameter (d) taken to be the centre of the sieved range. The Sauter mean diameter (e.g., Breard et al., 2019) is the most suitable diameter for considering the balance between particle weight and fluid drag, but as the samples are well-sorted, the arithmetic, geometric and Sauter means are within a few percent (based on measurements

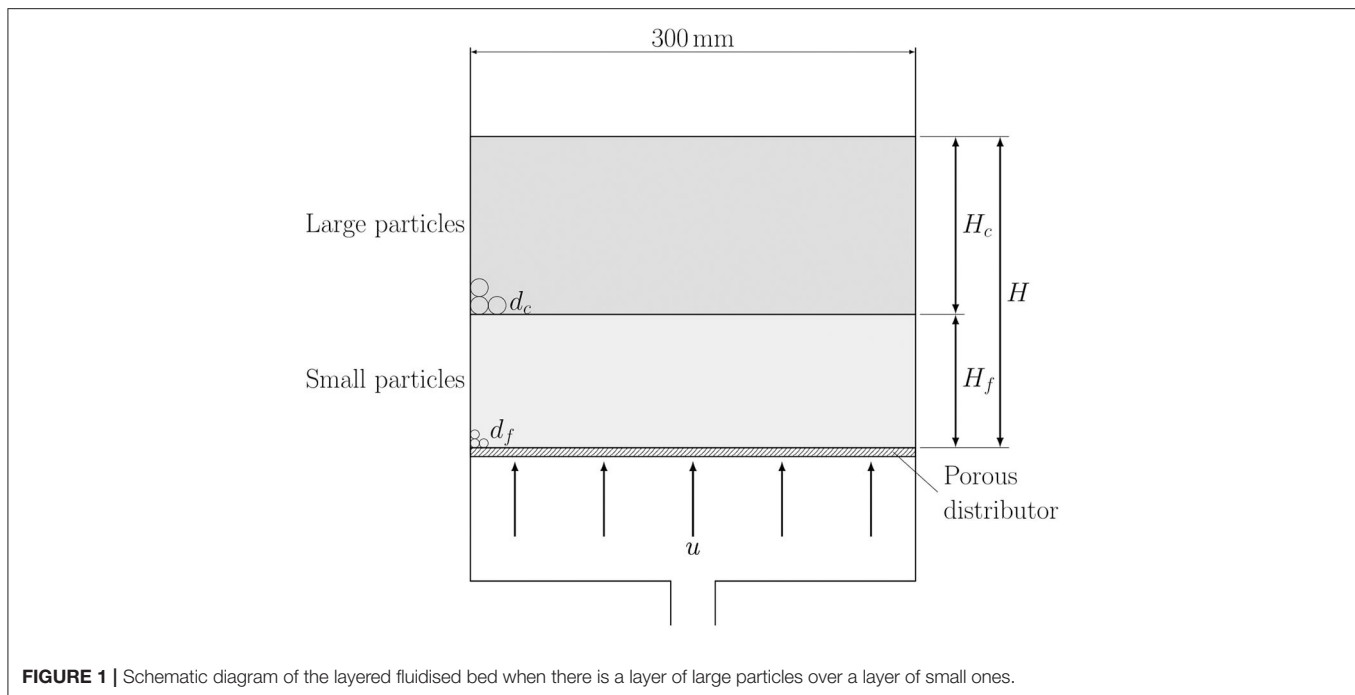


FIGURE 1 | Schematic diagram of the layered fluidised bed when there is a layer of large particles over a layer of small ones.

TABLE 1 | Particles used for two-layer beds with mono-sized particles.

<i>r</i>	Lower layer		Upper layer	
	Range (μm)	d_f (μm)	Range (μm)	d_c (μm)
2.67	125–250	188	400–600	500
5.63	45–75	60	250–425	338
8.33	45–75	60	400–600	500
10.08	45–75	60	510–700	605

r is the ratio of the diameter of the large particles in the top layer, d_c , to that of the small particles in the bottom layer, d_f .

of other batches of ballotini in the same laboratory), and we have taken this into account in our errors.

The total bed depth (H) was varied, with a maximum of 12 cm; the thickness of the component layers of the bed, and the sizes of particles in those layers were also varied. In all experiments the superficial gas velocity u (the volume flow rate per unit cross-sectional area of the bed) was increased incrementally and the behaviour of the particle layers observed through the transparent container walls. For some experiments pressure in the air near the base of the bed was determined with a metal tube attached to a manometer.

Most experiments began with a two-layer bed with each layer consisting of single particle components. The combinations of particle sizes tested are shown in **Table 1**. In a subset of these experiments the total bed depth (H) was kept constant at 10 cm but the coarse layer thickness (H_c) was varied as well as particle sizes in the two layers and therefore the size ratio $r = d_c/d_f$, where the subscripts c and f refer to the coarse and fine particle layers respectively. A second subset of experiments consisted

of a lower layer of 45–75 μm particles and an upper layer of particles with a diameter of 250–425 μm while H_c and H_c/H were varied systematically. A set of preliminary experiments explored the dynamics for three-layered beds with either a fine layer between two coarse layers or a coarse layer between two fine layers. In these experiments each layer contained a single particle size.

Experiments were also performed with two-layer beds consisting of mixtures of particles, where each layer contained two particle components, one large with a diameter d_l and one small, diameter d_s . The diameter for each layer was then determined by calculating the Sauter mean diameter, d_{av} , which preserves the ratio between volume and surface area for the particles. In general, for a bi-modal mixture this is given by

$$\frac{1}{d_{av}} = \frac{x_s/z_s}{d_s} + \frac{(1-x_s)/z_l}{d_l}, \quad (1)$$

where x_s is the mass fraction of the smaller component in the mixture, and the density ratio for component i is

$$z_i = \frac{\rho_i}{\rho_{av}}, \quad (2)$$

with the average density given by

$$\frac{1}{\rho_{av}} = \frac{x_s}{\rho_s} + \frac{1-x_s}{\rho_l}. \quad (3)$$

For particles of the same density, this reduces to

$$\frac{1}{d_{av}} = \frac{x_s}{d_s} + \frac{1-x_s}{d_l}. \quad (4)$$

TABLE 2 | Particles used for two-layer beds where each layer is a mixture of particles.

r	Lower layer					Upper layer				
	x_s	d_s	d_l	d_f	ϕ_f	x_s	d_s	d_l	d_c	ϕ_c
1.32	0.6	60	338	89	0.73	0.4	60	338	118	0.71
2.44	0.8	60	338	72	0.70	0.2	60	338	175	0.65
2.93	0.8	60	605	73	0.73	0.2	60	605	214	0.64
6.18	0.8	60	338	72	0.70	0.2	215	605	444	0.64

Particle volume fraction ϕ is calculated using the linear-mixture model of Yu and Standish (1991). x_s is the mass fraction of the smaller particles in each layer. d_s and d_l are the mean diameters of the small and large components in a layer, respectively. d_f and d_c are the Sauter mean diameter for the lower and upper layers, respectively. All diameters are in μm .

The particle volume fraction, ϕ , of mixtures was calculated with the linear-mixture method of Yu and Standish (1991) for randomly-packed mixtures of spherical particles; ϕ depends on the particle size ratio of the components of the mixture, d_s/d_l , and has better packing than mono-sized beds when $d_s/d_l < 0.741$. The mixtures used and the resulting values of d_{av} and ϕ for each layer are shown in Table 2.

3. OBSERVATIONS

3.1. Fine Particles on Top of Coarse Particles

When a layer of large particles (high permeability) is on the bottom and covered by a layer of small particles (low permeability), we were unable to find any experiment conditions (gas flow rate, layer thicknesses) with our apparatus and particles for which static-pressure failure or crater formation occurred. For this configuration, as the gas velocity was increased there was no particle motion until u_{mf} for the top layer was reached and the top layer fluidised. At this point all the small particles were in motion and gas bubbles rose through the fine-particle layer. However, these motions did not disturb the bottom (coarse) layer, which remained undeformed and acted as a type of distributor (i.e., the behaviour of the top layer was the same as if it were the only layer in the container and was directly on the distributor plate at the base of the container). Nothing further took place until u_{mf} for the large particles was reached and it was fluidised, causing mixing of the layers.

3.2. Coarse Particles on Top of Fine Particles

A much greater diversity of behaviour is seen for gas flows up through beds of particles with a layer of larger particles on top of a layer of smaller particles. The situation is shown schematically in Figure 1.

3.2.1. Jetting and Bubbling

For beds where $r (= d_c/d_f) < 6.5$, as u was increased, a velocity u_i is reached at which activity initiates. Initially, a longitudinal gas pocket formed within the bottom fine particle layer similar to those seen in the liquid-fluidised beds of Nichols et al. (1994). The

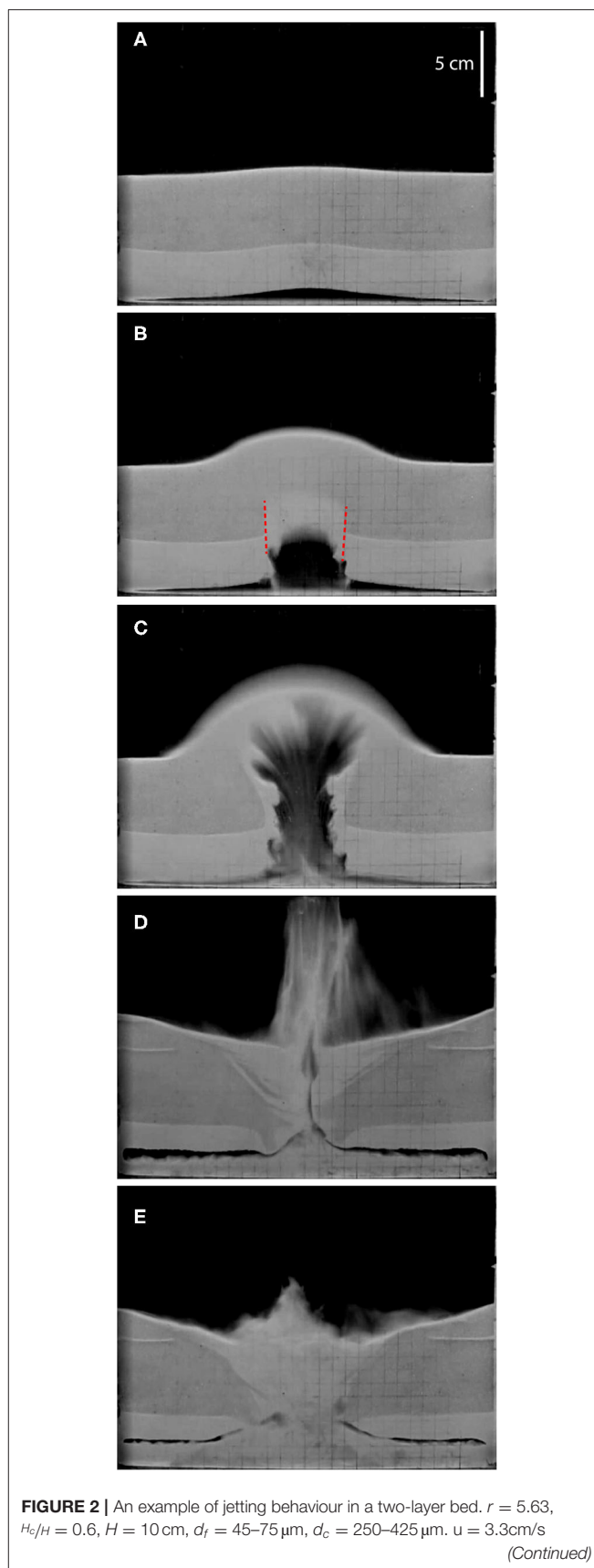


FIGURE 2 | An example of jetting behaviour in a two-layer bed. $r = 5.63$, $H_c/H = 0.6$, $H = 10$ cm, $d_f = 45\text{--}75\ \mu\text{m}$, $d_c = 250\text{--}425\ \mu\text{m}$. $u = 3.3\text{ cm/s}$

(Continued)

FIGURE 2 | and photographs (B–E) were taken 0.5 s, 1.0 s, 3.0 s, and 5.0 s after (A). The experiment started with a layer of coarser particles (darker) over a layer of finer particles (lighter grey); the lighter-grey at the top of (A) relates to lighting at the top of the coarser layer. The red lines in (B) indicate apparent planes of failure in the bed.

upper part of the layer of small particles was forced up against the layer of larger particles forming a double layer. This double layer deformed while maintaining the same thickness until the upper (coarse) layer of the bed is penetrated by the lower layer. This penetration could have the form of a jet or bubbles.

Jetting is shown in **Figure 2**. After initiation and the formation of a pocket, a column of fine particles intruded into the upper layer of large particles and a large cavity formed below it (both sometimes inclined). There appeared to be mechanical failure of the bed at the edges of the cavity. The top layer then suddenly failed and was penetrated and then broken through, causing particles to be projected above the bed and forming a jet of fine particles. While gas continued to be input at the base of the tank, the penetrating column of small particles widened and a stable, conical, bubbling pit of fine particles formed. In the example in **Figure 2**, before the breakthrough, the entire bottom layer was pushed up against the top layer and was not fluidised; however, after breakthrough only a portion of the fine layer pushed up on the base of the coarse layer, the rest formed a bubbling fluidised bed at the base of the tank.

An example of bubbling is shown in **Figure 3**. Many aspects of the bubbling regime were identical to jetting, but instead of a single cavity forming below the intruded column of small particles, smaller bubbles formed in the intrusion. When the top layer was breached, there was an overflow of small particles on top of the top layer, which broke up into blocks and sank. The crater area was dominated by bubbling. On some occasions this type of behaviour could be quite violent (“bubbles-jets”) with a plume of particles being thrown above the bed.

When either of the layers was very thin compared with the other (H_c or $H_f = 1$ cm), the bed could just become wholly fluidised as for a bed of single-sized particles.

There was no evidence seen of a large-scale expansion of the layers with increasing u ; instead structures largely void of particles—the pocket, jets, bubbles—formed, even for 45–75 μm particles for which some expansion might be expected (Geldart, 1973). If the gas flow into the base of the apparatus was ceased while there was a gas pocket in the lower layer but before breakthrough, the pocket simply collapsed non-dramatically.

3.2.2. Strength of Breakthrough

The strength of the breakthrough of gas and fines through the top layer is important in connection with behaviour (jetting, bubbling, bubble-jets). The type of behaviour and its strength, based on the maximum height attained by the ejected particles, is plotted out for beds of a fixed depth (H) and different values of r in **Figure 4**. The type of activity observed is indicative, and repeat tests showed it could differ for the same nominal conditions

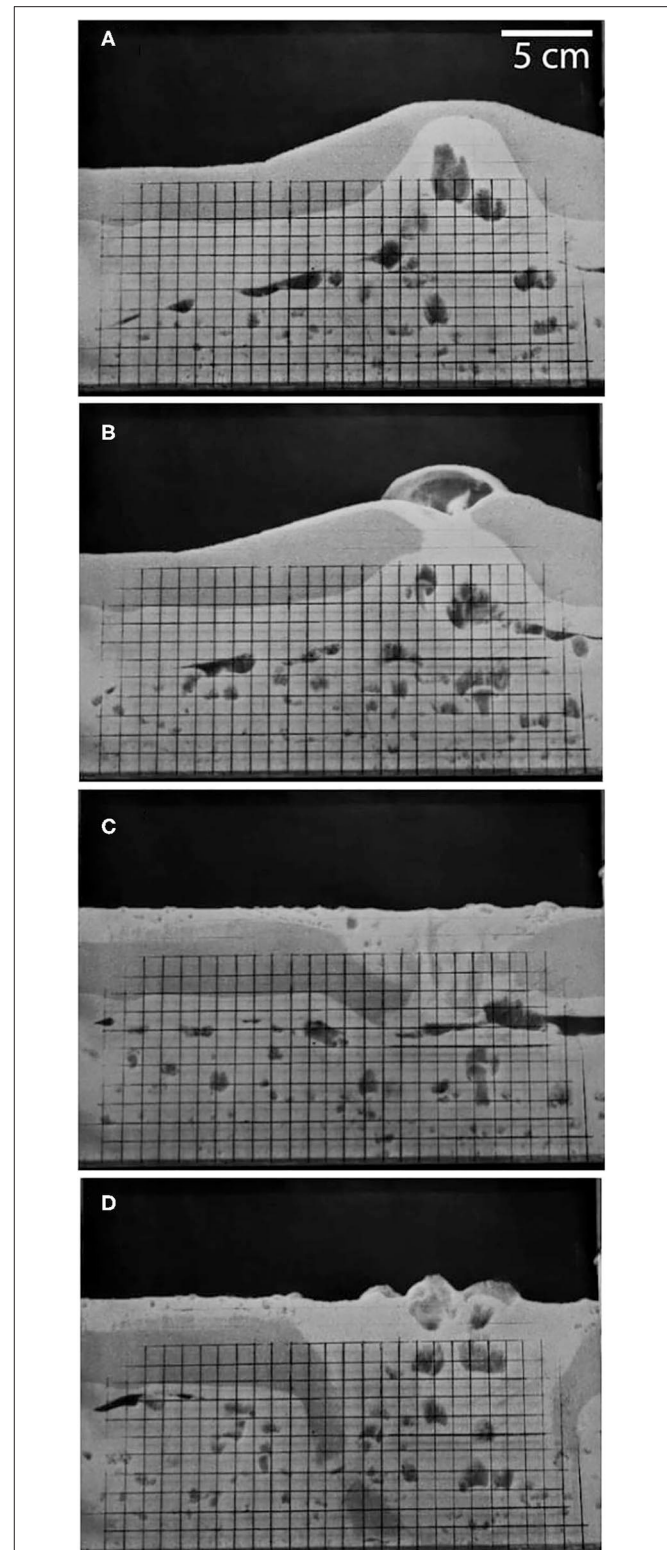


FIGURE 3 | An example of bubbling behaviour in a two-layer bed showing the progression with time from after initiation (A) to breakthrough (B) and further bubbling of fines (lighter grey) as gas continues to flow through the bed (C then D). $r = 2.67$, $H_c/H = 0.25$, $H = 12$ cm, $d_f = 125\text{--}250\text{ }\mu\text{m}$, $d_c = 400\text{--}600\text{ }\mu\text{m}$. The dark lines are a cm grid drawn on the front of the tank.

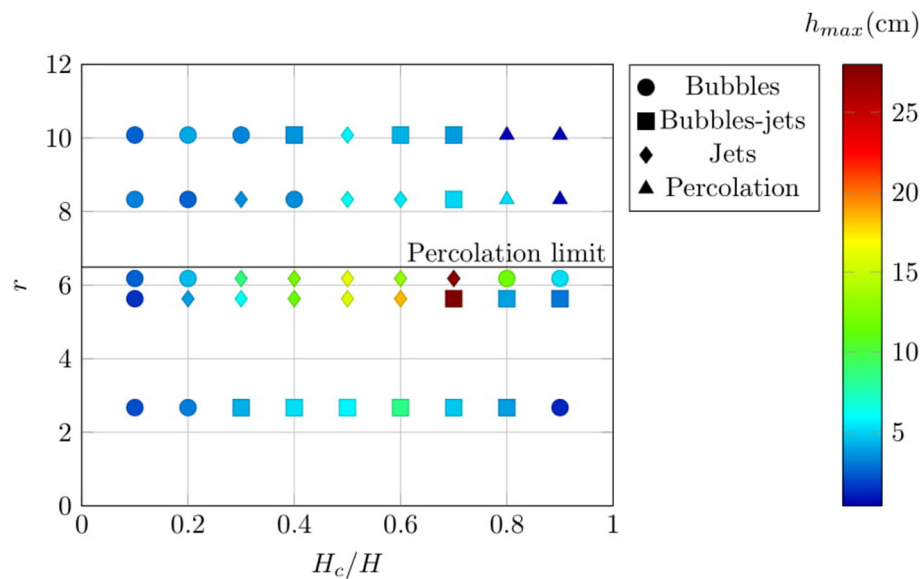


FIGURE 4 | The observed activity type in two-layer planar beds for different particle size ratios r , different coarse layer thicknesses (H_c) and constant total bed thickness (H) of 10 cm. Colours indicate the maximum height particles are ejected above the top of the bed (h_{max}). The nine points for $r = 6.18$ correspond to experiments where both layers were formed from a mixture of two particle sizes (bimodal); all other data are for experiments with unimodal layers. The percolation limit, i.e., the value for r above which small particles can move through the interstices of large particles, is 6.5 (Yu and Standish, 1991).

for some of the beds. However, jetting was more prevalent than bubbling for middling values of H_c/H and higher values of r . The strength of the breakthrough appeared to be highest for middling values of H_c/H but for all H_c/H it was diminished when r exceeded the percolation limit that permitted infiltration of fine particles into the coarse layer (see section 3.2.3 below) when jets could still take place but their vigour was significantly diminished. When the coarse layer was too thin then the void would not grow sufficiently to cause a jet to form; when it was too thick then the void could not grow sufficiently on its own to rupture the coarse layer.

After breakthrough, in the central part of the bed where breakthrough took place there appeared to be a region largely composed of fine particles which is fully fluidised. Away from this region, the layered structure of the bed was preserved though there might be some distortion and as for Nichols et al. (1994) some coarse particles passed downwards into the fluidised layer of fine particles below. A second layer of fine particles could form on top of the coarse layer owing to the fine particles that pass through the breakthrough region.

3.2.3. Percolation

A third type of behaviour occurred when a layer of large particles was over a layer of small ones when the small particles were sufficiently small relative to the large particles and $u_{mf} < u < u_{mf_c}$. In this case, the formation of the pocket after initiation did not take place, but the small particles travelled through the interstices between the large particles, percolating between them as shown in Figure 5. This would happen when $r > 6.5$ (Yu and Standish, 1991) for a packed bed. Vertical

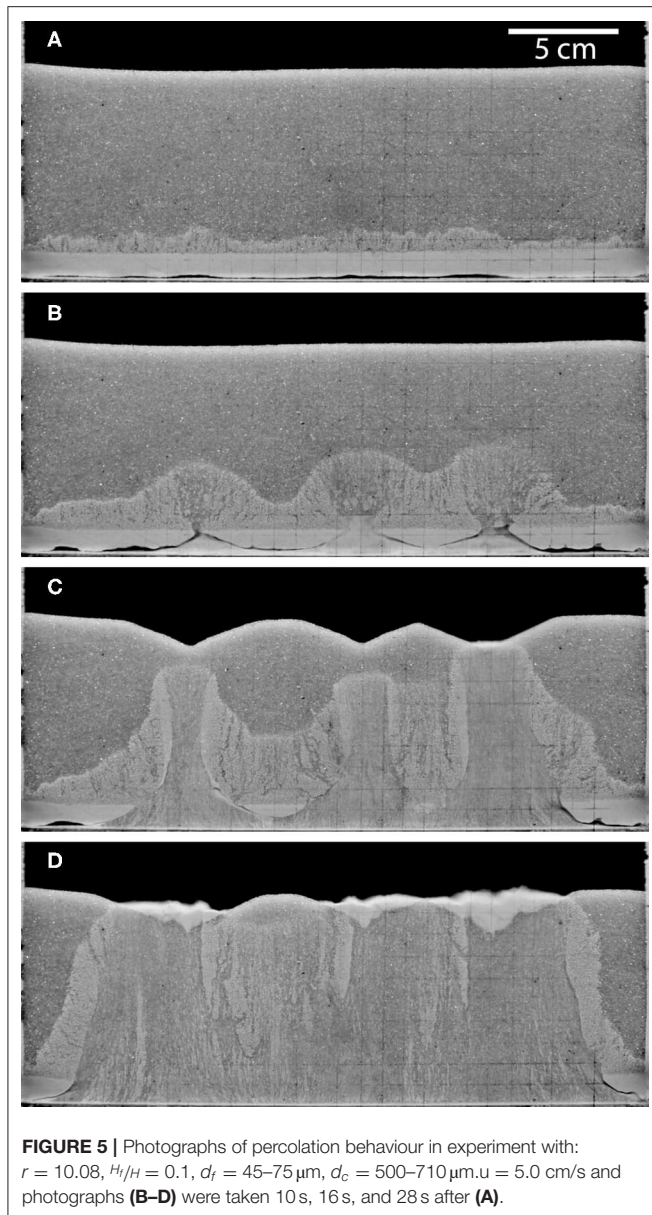
columns that were evacuated of small particles formed relatively slowly as for Gilbertson and Eames (2001) and Nermoen et al. (2010). These acted as high-permeability conduits for gas and so suppressed bubbling (Gilbertson and Eames, 2001) and there was no projection of particles above the bed. Small particles were transported through the spaces between the large particles to the top of the bed where they form a shallow pool.

3.2.4. Three-Layer Beds

Experiments were also performed in beds of three layers of unimodal spheres, always with $u < u_{mf_c}$. When a fine layer was between two coarse layers, the experiment proceeded in the upper two layers as if the bottom layer was not present: as u was incremented, a void formed in the fine layer and the top coarse layer was lifted until it failed. The particles in the bottom coarse layer did not move (i.e., the bottom layer acted as a distributor). When a coarse layer was between two layers containing the same fine particles, the upper layer behaved like an ordinary fluidised bed, and the behaviour of the lower-two layers was similar to the equivalent experiment with just those two layers.

4. FLUID FORCES ON LAYERED PARTICLE BEDS

Although uniform gas flow up through a layered bed of particles is a simple system, there is a rich variety of behaviour possible through the interaction between many different physical processes. Following the work of Nichols et al. (1994), the driving mechanism behind the deformation and rupture of the layers is the drag exerted on the particles by the passage of fluid past it.



This exerts a force on the particles directly, but also can change the interaction of particles.

4.1. Fluidisation in Beds of Particles of a Single Size

For a bed of uniform particles of diameter d and density ρ_p , when there is a flow of fluid of superficial velocity u through it, the forces on the bed are the particles' net weight and the drag exerted on them. The drag is considerably larger than that on a single isolated particle owing to the presence of nearby, surrounding particles. As the fluid flow through a bed of single-sized particles is increased, the drag on the particles increases. Eventually the minimum fluidisation velocity, u_{mf} , is reached when drag balances the net weight of the bed. For mono-sized

particles, this is also the point at which the weight of individual particles is supported and inter-particle friction is eliminated so that the bed behaves in a similar manner to a fluid. A simple way of expressing this balance is the semi-empirical Ergun equation (Ergun, 1952)

$$\frac{1.75\phi}{(1-\phi)^3} \frac{\rho_f H}{d} u_{mf}^2 + \frac{150\phi^2}{(1-\phi)^3} \frac{\mu H}{d^2} u_{mf} = \phi \Delta \rho g H, \quad (5)$$

where ϕ is the particle volume fraction of the bed, μ is the viscosity of the fluid, $\Delta \rho$ is the difference between the particle and the fluid densities, and H is the depth of the bed. u_{mf} is a superficial velocity and so the actual average velocity within the bed is u_{mf}/ϕ . The left-hand side of the equation expresses the drag on the particles. A heuristic approach is taken summing the first term representing the inertial force to the second term representing the viscous force. The right-hand side of the equation is the net weight of the bed. It may be written in non-dimensional form as

$$P Re_{mf}^2 + Q Re_{mf} - Ar = 0, \quad (6)$$

where Re_{mf} is the particle Reynolds number (the ratio between inertial and viscous forces on a particle) at $u = u_{mf}$,

$$Re_{mf} = \frac{\rho u_{mf} d}{\mu},$$

and Ar is the Archimedes number

$$Ar = \frac{\Delta \rho \rho d^3 g}{\mu^2},$$

the ratio of net weight to viscous forces, and a function of particle and fluid properties only. P and Q define the effect that the close proximity of particles has on drag in the bed and so are functions of ϕ . They are defined by

$$P = \frac{1.75}{(1-\phi)^3}, \quad Q = \frac{150\phi}{(1-\phi)^3}.$$

They may be related to inertial permeability ($= d/P$) and viscous (Darcian) permeability ($= d^2/Q$).

Above the velocity of minimum fluidisation the net weight and the drag on the particles remain balanced. For particles that are not too small or light (Geldart, 1973), the excess gas flow is concentrated forming voids or “bubbles” in the bed that pass up through it (Davidson and Harrison, 1963). These bubbles can coalesce and divide, and also drive circulation currents of particles within the bed.

Fluidisation in a mono-sized bed of particles is idealised as a discrete event: it takes place at the gas velocity when at the bed scale the drag balances the net weight of the particles and at the particle scale inter-particle friction is practically eliminated. It is assumed that the drag on all the particles is the same for a given gas velocity and for each particle the only net vertical forces acting on it are its net weight and drag.

4.1.1. Fluidisation in a Two-Layer Bed

When a bed consists of two layers of particles, its fluidisation behaviour can be much more complicated. The minimum fluidisation velocity depends on the size and density of particles, and so from the point of view of individual particles, when there are two layers of different particles in a bed there will be an interval of fluid velocities over which the particles of one set will be fluidised and the other set will not be. The particles used in our experiments were differentiated by size only (density was constant) and so will be referred to as coarse and fine particles, but this is a proxy for referring to particles in a bed in which one set of particles has a higher value of u_{mf} than the other. In addition, the discussion below is for sets of particles for which r is not sufficiently large to allow particle percolation.

When a two-layer bed consists of a layer of coarse particles overlaid by a layer of fine particles, then the observed behaviour was straightforward as described in section 3.1.

More complex behaviour is seen when small u_{mf} particles form the lower layer and large u_{mf} particles the upper one. As for the opposite case (fine layer on top), as the fluid flow rate is increased it reaches the minimum fluidisation velocity for the fine particles; however, in this configuration the entire layer of small u_{mf} particles cannot be fluidised owing to the weight of the still unfluidised top layer of large u_{mf} particles. This causes a division of the fine-particle layer with a static upper part forced up against the upper layer and a lower part that is fluidised (Nichols et al., 1994): the drag exerted on the upper part of the fine-particle layer supports the weight of the small u_{mf} particles composing it and the excess drag (i.e., the total drag on the fine particles minus the drag to support the weight of the fine particles) supports the effective weight of the upper layer (Nichols et al., 1994). In this state, the weight of the upper layer of the bed (composed of coarser and so larger u_{mf} particles) is fully supported by the gas flow, but individual particles are not fluidised and there is significant friction between them; the same is true of the upper part of the layer of fine particles where the excess drag forces the particles together and so there is a frictional force between them. The particles in the lower part of the layer of fine particles (below the gas pocket) are fully fluidised i.e., the weight of the particles is fully supported and the inter-particle friction is insignificant.

A schematic diagram of the bed at the point at which the weight of the top layer is fully supported is shown in **Figure 6**. From the point of view of fluid drag, it is possible to estimate for a given gas velocity the thickness, H_f^* , of the upper part of the layer of low u_{mf} particles required to support the weight of the upper layer of large u_{mf} particles. From the Ergun equation, Equation (5), summing the pressure drop through the two parts of the composite layer gives

$$P \left(\frac{H_c}{d_c} + \frac{H_f^*}{d_f} \right) \rho_f u_{mf,bed}^2 + Q \left(\frac{H_c}{d_c^2} + \frac{H_f^*}{d_f^2} \right) \mu u_{mf,bed} = \Delta \rho_c g H_c + \Delta \rho_f g H_f^*, \quad (7)$$

where $u_{mf,bed}$ is the superficial velocity at which the weight of the upper layer is supported, and $\Delta \rho$ is the difference between the density of the particles and that of the surrounding fluid. The

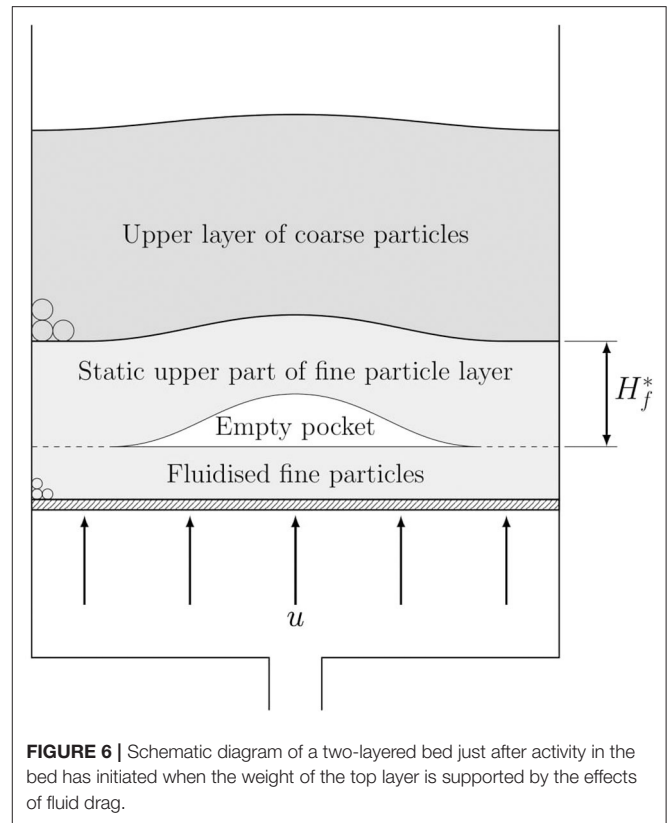


FIGURE 6 | Schematic diagram of a two-layered bed just after activity in the bed has initiated when the weight of the top layer is supported by the effects of fluid drag.

Ergun equation accommodates both drag and hydrostatic forces, the latter accounting for a factor of $(1 - \phi)$ in the denominator of both P and Q . The particle volume fraction ϕ is assumed to be uniform throughout the composite layer. This expression includes the effects of inertia, which were neglected by Nichols et al. (1994).

Equation (7) may be non-dimensionalised so that

$$PRe_c^2 (H'_c(1 - r) + r) + QRe_c (H'_c(1 - r^2) + r^2) - (H'_c(1 - 1/w) + 1/w) Ar_c = 0, \quad (8)$$

where Re_c is calculated when $u = u_{mf,bed}$, $H'_c = H_c/H_c + H_f^*$, the relative thickness of the layer of coarse particles, and the density difference ratio $w = \Delta \rho_c / \Delta \rho_f$.

For a given H'_c , this equation may be solved implicitly to obtain the corresponding $u_{mf,bed}$, the gas velocity at which the net weight of the upper layer is balanced by fluid flow drag. For a given $u_{mf,bed}$ then

$$H'_c = \frac{Ar_c/w - rPRe_c^2 - r^2QRe_c}{PRe_c^2(1 - r) + QRe_c(1 - r^2) - ((1 - 1/w)Ar_c)} \quad (9)$$

or, when all the particles have the same density so that $w = 1$,

$$H'_c = \frac{Ar_c - rPRe_c^2 - r^2QRe_c}{PRe_c^2(1 - r) + QRe_c(1 - r^2)}. \quad (10)$$

These equations are wholly in terms of the large particles: the properties of the small particle layer enter only through r . The

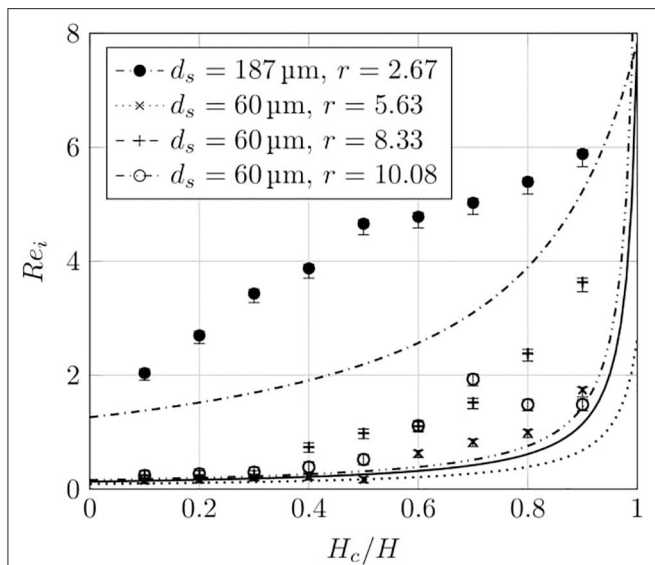


FIGURE 7 | Variation of the Reynolds number of the large particles at the point of initiation of the formation of a pocket in the lower, fine particle layer of the bed. The initial thickness of the bed was 10 cm for all the beds. Curves are Equation (10), which relates Re and H_c/H at $u = u_{mf}$; points are experimental measurements.

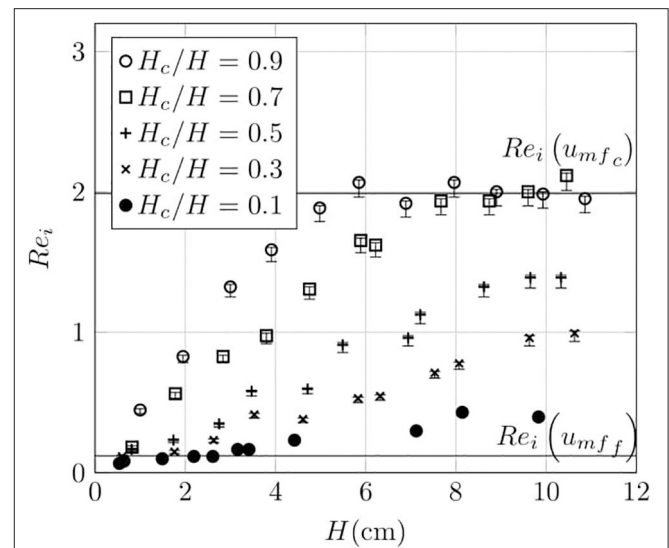


FIGURE 8 | Initiation Reynolds number as a function of H for the larger particles in two-layer fluidised beds consisting of a lower layer of particles with diameters 45–75 μm and an upper layer of particles with diameters of 250–425 μm for five H_c/H values. The two black horizontal lines indicate the two Reynolds numbers corresponding to the minimum fluidisation velocities, u_{mf} and $u_{mf,c}$, determined experimentally with mono-sized fluidised beds of each component with a depth of 4 cm.

value of H'_c given by Equation (10) is a minimum value. In a system where u is steadily incremented, the value of H'_c required from Equation (10) will decrease as more of the weight of the coarse particles is supported directly by the flow through drag, but there is no mechanism by which fine particles can detach themselves from the double layer and so there will be a net upward force on the double layer.

4.2. Initiation of Activity in Layered Beds of Mono-Sized Particles

When the weight of the upper layer of the bed is supported, then it can start to deform, allowing the pocket to form in the lower layer of the bed. $u_{mf,bed}$ can therefore be identified with the point at which deformation in the bed is first observed; we call this the initiation velocity u_i with corresponding particle Reynolds number, $Re_i = \rho_g u_i d_c / \mu$. Equation (10) is plotted out in **Figure 7** along with experimental data for the first sub-set of experiments (fixed $H = 10$ cm). For the small-scale experiments, H_f has been used to calculate H'_c . H_f^* was measured for the second sub-set of experiments (fixed $r = 5.63$). Neglecting the case when either layer was very thin (H_c or $H_f = 1$ cm), the mean relative thickness of the layer was $H_f^*/H_f = 0.87$ with a standard deviation of 0.10; therefore it is reasonable to identify H'_c with H_c/H . When $H'_c = 1$ then $Re_i = Re_{mf,c}$.

It is apparent that even a thin bottom layer of fine particles is sufficient to greatly increase the fluid force on the upper layer of large particles and cause a sharp drop in the expected value of Re_i . In the model, e.g., Equation (10), r controls the concavity of the curve, while the endpoints are controlled by the minimum fluidisation velocities for the fine and coarse particles

alone. Many aspects of the theoretical curves are captured by the experimental measurements; however, the theory consistently under-predicts the Reynolds numbers at which initiation occurs in the experimental beds.

In the second sub-set of experiments there was a lower layer of 60 μm particles and an upper layer of particles with a diameter of 338 μm . Their particle size ratio $r = 5.63$ corresponded to some of the most energetic breakthroughs seen in the first sub-set of experiments. **Figure 8** shows the Reynolds number for the initiation of activity with overall bed depth for sets of experiments where H'_c was kept constant. It can be seen that Re_i depends strongly on H_c/H , as would be expected from Equation (7); however, if the activity in the bed was solely determined by the balance between weight and fluid drag then Re_i should be a constant for a given value of H_c/H ; in fact there is a clear dependence on H , or perhaps $H_c + H_f^*$. There are signs that this levels out for deeper beds, but at values of Re_i that are significantly in excess of what would be expected from Equation (7). For the largest values of H_c/H , the levelling-off occurs when the value of $Re_{ic} = Re_{mf,c}$.

4.2.1. Initiation of Activity for Two Layers of Particle Mixtures

Geological materials are rarely composed of a single component. Two-layer beds where each layer was composed of a mixture of particles as detailed in **Table 2** were therefore examined. Each mixture consisted of a small component (subscript s) and a large component (subscript l). When calculating the drag, the Sauter mean diameter (4) is the most suitable diameter (van der Hoef

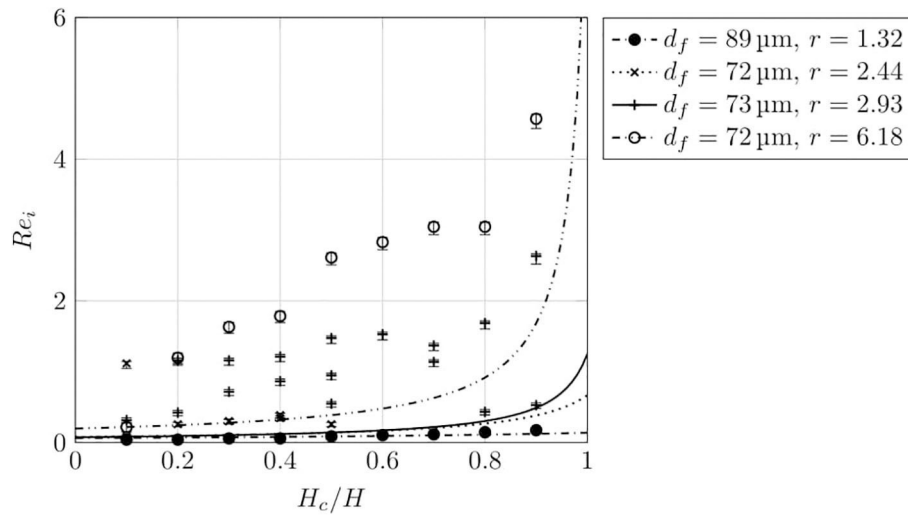


FIGURE 9 | Dependence of initiation Reynolds number on relative coarse layer thickness for several beds consisting of mixtures of particles as specified in **Table 2**. All the beds had an overall thickness $H = 10$ cm. The curves describe Equation 10 and the points are experimental measurements.

et al., 2005) and its value for the upper layer is the diameter that is used in Re_c and Ar_c . The mixing of particles can also allow better packing and so increase the drag experienced by the bed. The effect of packing in Equation (8) is determined by P and Q , and as ϕ will now be different in the upper and lower layers of the bed, then P and Q will also differ. Equation (8) therefore becomes

$$Re_c^2 (P_f H'_c (1 - r) + P_c r) + Re_c (Q_f H'_c (1 - r^2) + Q_c r^2) - (H'_c (1 - 1/w) + 1/w) Ar_c = 0. \quad (11)$$

ϕ_f and ϕ_c can be estimated using a linear-mixture model (Yu and Standish, 1991; Yu and Zou, 1998), and the values for the mixtures used are listed in **Table 2**. From these, P and Q may be calculated for each layer and the equation solved for Re_c .

The same types of behaviour were seen for layers that are bi-modal mixtures of particles as for the layers of mono-sized particles, except that for the mixtures tested, jetting was seen more often than for the mono-sized layered beds. For $r = 6.18$, the maximum height of ejected particles was also measured and these results are plotted in **Figure 4**, and it can be seen that the types of activity and the strength of breakthrough were comparable to the beds of mono-sized layers.

Figure 9 shows the Reynolds number at which activity initiates. The trends are the same as for the mono-sized (non-mixed) layers shown in **Figure 7** including the significant under-prediction of the initiation Reynolds numbers by the theory based on fluidisation, Equation (10).

4.3. Breakthrough for Layered Beds

After initiation, H_f^* is maintained as there is no mechanism by which fine particles may be detached from it. This generates an excess drag on the layer of coarse particles and the immobile top part of the layer of fine particles, and so they are forced

upwards to form the longitudinal air pocket. This pocket was typically centred within the tank, though on some occasions an asymmetrical pocket formed. A void above the pocket grew with increments of u until there was a sudden breakthrough of the lower layer through the upper layer in the form of bubbles or a jet.

For the set of experiments when H_c/H was kept constant, the breakthrough of the upper layer took place when $u \approx 1.2u_i$. In a conventional fluidised bed with a single layer of particles, the pressure drop over the bed would rise until it matched the weight of the bed and then level off (Davidson and Harrison, 1963); however, in our experiments for a two-layer bed with $u_{mf_c} > u_{mf_f}$ there was a steady pressure rise to a value significantly in excess of the weight of the bed until breakthrough. When breakthrough occurred, there was a sudden drop in pressure to a value close to that corresponding to the weight of the bed.

Figure 10 shows a typical pressure drop over a bed, recorded using a manometer with an outlet positioned at the bottom of the bed (i.e., just above the distributor plate). The pressures measured are steady pressures i.e., after each increment of u , the pressure was allowed to come to an equilibrium value. When $u = 4$ cm/s, the estimated pressure drop over the bed owing to drag calculated from terms equivalent to the first two terms of Equation (11) was 7200 Pa compared to the 6000 Pa measured. Some difference would be expected owing to the distortion of the particle layers at breakthrough, but this gives some confidence that the force exerted on the particles is dominated by drag.

The strength of breakthrough, as indicated by the maximum height of the particles ejected from the bed, is shown in **Figure 11** for five sets of experiments from the second sub-set for which H_c/H is constant. There is a similar dependency in the strength of the breakthrough on H_c/H with the strongest breakthroughs for middle values; however, there is a dependence on H in absolute terms as well.

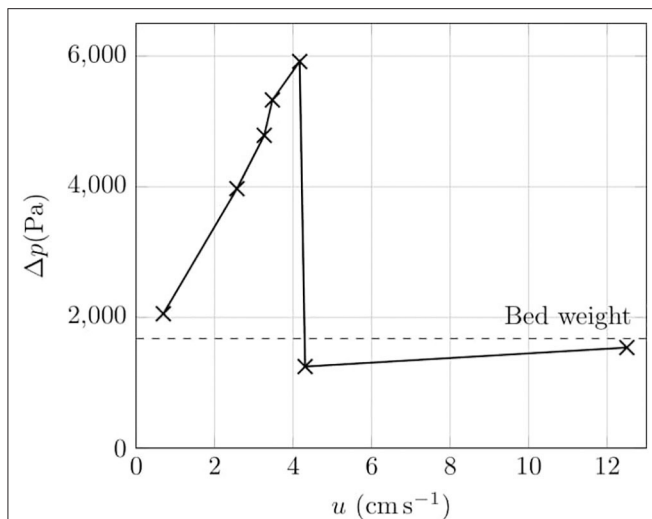


FIGURE 10 | Change of pressure drop over a two-layer bed as u is incremented. The sudden fall in pressure corresponds to the point at which breakthrough takes place. The total bed thickness was 10 cm and the bed layers conformed to $r = 2.44$ in Table 2. The dashed line is the bed weight calculated as $\phi_c \Delta \rho_c g H_c + \phi_l \Delta \rho_l g H_l$. $H_c/H = 0.6$.

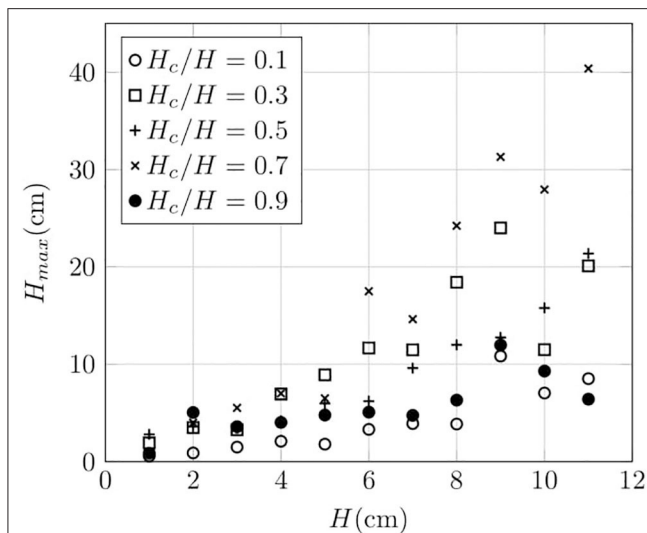


FIGURE 11 | Strength of breakthrough for a two-layer fluidised bed where H_{max} is the maximum observed height of particles ejected from the bed. Heights were measured to an accuracy of ± 0.1 cm. The bed consisted of a lower layer of particles with diameters 45–75 μm particles and an upper layer of particles with a diameters 250–425 μm where H_c/H is kept constant over a range of H for five values of H_c/H .

5. DISCUSSION

The established conceptual model of secondary hydroeruptions through hot pyroclastic flow deposits (e.g., Moyer and Swanson, 1987) emphasises the role of permeability (fine grain size) in the primary deposit. In this model, which we term “static pressure build-up,” the low permeability reduces the rate of

steam escape enabling the underlying steam source to pressurise until the overburden fails, triggering the secondary eruption. However, for any non-zero permeability, if the pressure at the steam source increases, so will the flow up through the interstices of the deposit, increasing the drag force pushing upwards throughout the entire deposit thickness. We propose an alternative model where drag is fundamental to triggering secondary hydroeruptions. It is suitable for deposits that are effectively granular materials for which the permeability is high enough for the drag force to be comparable to the static pressure force; it is not relevant to secondary eruptions through welded deposits in which the particles will be stuck together regardless of the flow rate of gas. Our simple analogue experiments with uniform-density spherical particles demonstrate that upflow of gas from an underlying distributed source can cause localised violent outbursts of particles from the top of a bed of layered granular material.

Violent outbursts do not occur for single-layer beds or in two-layer beds where the capping layer is finer-grained (lower permeability) than the layer below it; however, if the layers are reversed so that the coarser-grained layer is on top, then jets of particles form for some gas fluxes and layer thicknesses and grain size contrasts. Our experiments and theoretical considerations, including those outlined in Nichols et al. (1994), indicate that what matters is not the permeability of the layers but the minimum gas velocity for drag to support the weight of the particles, u_{mf} . In the experiments we controlled u_{mf} through particle size and used spherical particles with unimodal or bimodal size distributions, which are well-studied in industrial applications and are the easiest to model and understand; however, in general u_{mf} will be determined by the size distribution, densities and shapes of particles making up a layer.

The violent breakthrough in layered systems where the top layer has a u_{mf} larger than that in the lower layer is enabled by the interaction between the two layers. The upper part of the lower layer of fine particles (above a gas pocket) supports the weight of the upper layer of coarse particles, forming a composite structure. In neither part of this composite are the particles individually fluidised because the gas flow is not large enough to fluidise the large particles, and the small particles are forced against the large ones by the excess drag on them. This ensures that there continues to be significant inter-particle friction and the composite has a strength so that the upstream pressure increases to a value in excess of the lithostatic. The theory based on fluidisation alone, Equation (10), underestimates Re_i for both mono-sized layers and mixed layers; this is consistent with the static strength of layers also playing a role in the initiation of activity. It is the arching of the bed (permitted by it having a strength) which forms a region with no particles. This gas pocket causes increased flow through its apex, locally fluidising the particles above. In this region where there is full fluidisation, jets and bubbles can form which further concentrate the flow. Once breakthrough is achieved, the central portion of the bed is fully fluidised and the pressure drop over it is suddenly reduced to that corresponding to the bed's weight, releasing the excess pressure. This transient, and the concentrated flow owing

to bubbles or a jet, generates the plume of particles expelled at breakthrough.

The analogue experiments and theoretical constraints indicate that the drag-induced triggering of secondary hydroeruptions pyroclastic deposits requires that:

- The deposit is a granular material with particles free to move relative to one another if the local gas flow is sufficient for the weights of particles to be supported. This means the primary deposit is not welded and has low cohesion.
- The deposit has some strength through friction in order to allow buildup of overpressure.
- The primary deposit is layered with vertical changes in u_{mf} .
- There is a layer with sufficiently low u_{mf} (e.g., it is sufficiently fine-grained) for the upwards velocity of steam generated by the thermal energy of the primary deposit to exceed it.
- This low- u_{mf} layer is overlaid by a layer with higher u_{mf} (e.g., due to coarser grain size and/or higher proportion of lithic clasts of high density).
- The low- u_{mf} layer is sufficiently thick compared to the thickness of the deposit above it to satisfy Equation (9).

5.1. Application to Deposits

To consider the above requirements and apply the insights from our analogue experiments to secondary hydroeruptions, we refer to the Mount St Helens (MSH) 1980 eruption. It has well-studied primary pyroclastic flow deposits (Kuntz et al., 1981; Rowley et al., 1981; Brand et al., 2014) and the best-documented secondary hydroeruptions (Rowley et al., 1981; Moyer and Swanson, 1987). That the deposits can be treated as low-strength granular materials that would fluidise with sufficiently fast upflow of gas is suggested by the “striking deformation” when people attempted to walk on the primary deposits in the weeks after emplacement (Wilson and Head, 1981) and the sloughing of the primary deposits into the secondary hydroeruption craters to form gentle slopes (Rowley et al., 1981). Based on the responses to loads on the top surface and shear vane tests in the upper channel deposit, Wilson and Head (1981) estimated a yield strength of $\sim 300\text{--}2,000\text{ N/m}^2$ and $400\text{--}18,000\text{ N/m}^2$, respectively. However, a degassed and compacted deposit (with degassing induced by loading experiments) was substantially stronger (e.g., it could support an adult standing on one foot), and they attributed much higher compressive strengths of $100,000\text{--}250,000\text{ N/m}^2$ determined from cone penetration to the efficiency of degassing induced by the steadily increasing force applied during these tests. We hypothesise that for the drag-induced triggering of secondary hydroeruptions, the increased strength with compaction demonstrates how the portion of the (fine-grained) layer where $u_{mf} < u$ can gain an appreciable strength when it is pushed up and is compacted against the weight of the overlying material with $u_{mf} > u$. The pressure that builds in the gas pocket, which contributes to the intensity of the outburst when the overlying material is breached, depends on the bending strength of the material above the pocket, and so although most of the deposit would be weak and easily deformed, the compaction induced by excess drag in the low u_{mf} part of the composite layer

above where the pocket initiated would allow greater pressure to accumulate.

Sections through the MSH May 18 pyroclastic flow deposits exposed along drainages by recent erosion that were studied by Brand et al. (2014) reveal that the primary deposits can be considered as layered with vertical changes in grain size and componentry, and so there are vertical variations in u_{mf} . Although the four main units (I, II, III, IV) of the May 18 pyroclastic flows have intricate vertical and lateral facies variations, the outcrop photographs and diagrams of Brand et al. (2014) show laterally continuous layering defined by grain size (and componentry) is common over distances of tens of metres. Lithofacies include: massive lapilli tuff; block-rich massive lapilli tuff, sometimes with block-rich basal breccia; pumice lens; fine-grained massive ash, up to tens of centimetres thick. There is considerable variation in median grain size and sorting (Kuntz et al., 1981; Brand et al., 2014): for example, the median of the samples sieved by Brand et al. (2014) 7.1–7.2 km from source vary from $< 100\text{ }\mu\text{m}$ to $> 10\text{ cm}$. The stratigraphic logs show that there is commonly a sudden increase in grain size with stratigraphic height across unit boundaries (e.g., from units II to III and from III to IV), which would correspond to vertical increases in u_{mf} .

The preservation of layers in the primary deposits, including close to secondary hydroeruption sites, means that the steam flux after emplacement was not sufficient to exceed u_{mf} of most (or all) of the deposit. However, for the proposed drag-induced triggering of secondary eruptions, there must be layer(s) where the steam velocity exceeded u_{mf} . **Figure 12** shows u_{mf} as a function of particle diameter for three particle fractions ($\phi = 0.5, 0.6, 0.7$) and two end-member particle densities that correspond to the typical pumice density (750 kg/m^3) and the bubble-free (glass and crystals) juvenile clast density ($2,550\text{ kg/m}^3$) determined by Kuntz et al. (1981). It indicates that the effects of the expected variations in density and particle volume fractions would usually be much less important than variations in grain size in their effects on variations of u_{mf} in pyroclastic flow deposits. For beds with a range of particle sizes (e.g., pyroclastic deposits), if the property of interest relates to drag (e.g., u_{mf} and permeability, Breard et al., 2019), then the relevant particle diameter is the Sauter mean diameter (Equation 4). The Sauter mean diameter is sensitive to the finer grain sizes and is always smaller than the median (by mass) when all the particles are considered to have the same density (and also when the fine particles are relatively dense).

Most of the secondary hydroeruptions occurred within a few days of emplacement of the May 18 pyroclastic flows. Moyer and Swanson (1987) include data on the grain size distribution of one May 18 pyroclastic flow sample down to $9\Phi \approx 2\text{ }\mu\text{m}$, with just 0.12 wt.% finer than 9Φ . Applying Equation (4) and using the geometric mean for the diameter of each particle size bin gives a Sauter mean diameter of $110\text{ }\mu\text{m}$. Breard et al. (2019) show how to estimate the Sauter mean diameter from the commonly reported Φ -scale based median (Md) and sorting (σ) parameters, assuming a log-normal particle size distribution. This gives a Sauter mean diameter of $97\text{ }\mu\text{m}$ for the same Moyer and Swanson (1987) sample, in good agreement with Equation (4). Applying

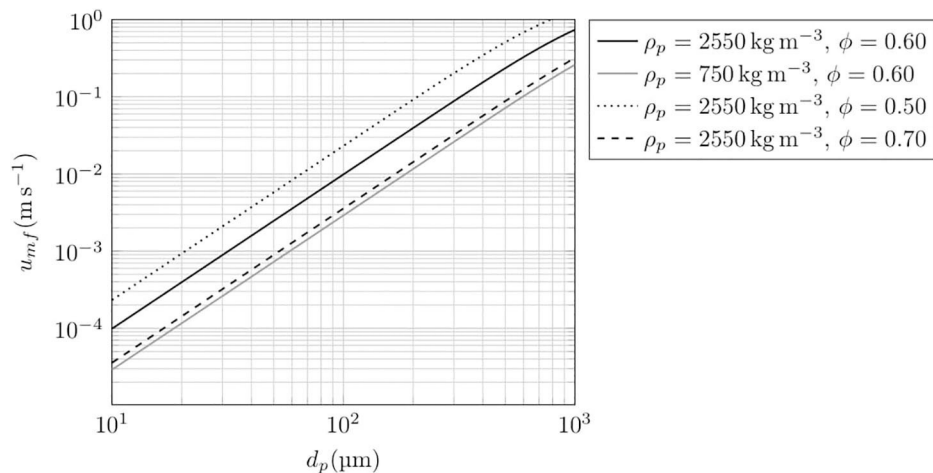


FIGURE 12 | Typical minimum fluidisation curves with particle diameter calculated from Equation (5) showing their sensitivity to particle density and particle volume fraction. The fluidising gas is superheated water vapour with a temperature of 250 °C: $\rho = 2.37 \text{ kg/m}^3$ and $\mu = 1.80 \times 10^{-5} \text{ kg/ms}$.

the Breard et al. (2019) approach to the nine May 18 pyroclastic flow size distributions in Kuntz et al. (1981) gives mean Sauter mean diameters of 55–206 μm . Data from the more extensive sampling of recent exposures of the May 18 units along drainages by Brand et al. (2014) suggest the Sauter mean diameter can range from < 10 microns to > 1 mm [c.f. Figure 4F of Brand et al. (2014) and Figure 9B of Breard et al. (2019)].

Figure 12 gives a sense of the implications of these grain size data for the ranges of u_{mf} in pyroclastic flow deposits. For example, for a density of 2,550 kg/m^3 , Sauter mean diameters of 55, 200, and 1,000 μm correspond to u_{mf} values (and the volume flux of steam generated per unit area) of $3 \times 10^{-3} \text{ m/s}$, $4 \times 10^{-2} \text{ m/s}$, and 0.7 m/s , respectively. These steam rates suggest that it is feasible for upflow of steam to overcome u_{mf} of some, but not most, of a pyroclastic flow deposit succession as required to trigger secondary hydroeruptions and preserve layered deposits. However, the argument would clearly be strengthened by modelling of steam generation and data on grain size and density from samples collected at the roots of secondary hydroeruptions, which are beyond the scope of this study.

In our laboratory experiments with layers of mono-sized particles, the intensity of outbursts of particles was substantially diminished when the ratio of the particle diameters of the two layers was sufficient for the smaller particles to percolate through the interstices of the coarser layer above. For these experiments this meant that violent outbursts were abated when $r > 6.5$. This will be partly because excess drag on the particles in the lower layer causes percolation rather than it being exerted against the upper layer. Also the mixing of the small and large particles causes u_{mf} for the upper layer to be decreased (Gilbertson, 2019). For natural pyroclastic deposits with much broader size distributions we expect percolation to be much less important because of the more efficient packing and smaller interstices than in mono-sized beds. In fluidised beds of mixtures, segregation often takes place owing to the difference in u_{mf} of the components (Gilbertson, 2019); however, this was not apparent

in experiments with mixtures of particles because the particles in the composite structure are not individually fluidised and they are not free to move. Thus we expect the intensity of outbursts to increase for greater r , even when $r > 6.5$, in pyroclastic deposits, with r based on the ratio of Sauter mean diameter of layers. Other factors that would affect intensity are the bending strength of the beds and the relative thickness of the layers; further work is required to make robust quantitative predictions of their roles.

The mechanism for triggering secondary hydroeruptions we have explored in this paper complements that proposed by Moyer and Swanson (1987) in that in both models steam pressure builds at depth before the deposit is breached causing a sudden pressure drop and eruption of steam and particles. The addition of the role of drag in our model means that the root of the secondary eruption is not necessarily at the depth of the steam source: it can, and generally would, be higher up in the deposit where there is a relatively low- u_{mf} layer. Moyer and Swanson (1987) proposed that the steam source for the MSH secondary hydroeruptions was pools of water on top of the May 18 debris avalanche deposit because of the dearth of the distinctive cryptodome dacite clasts from the debris avalanche in the secondary hydroeruption deposits. In our drag-related mechanism for secondary eruption triggering, the water could be in pools on top of the debris avalanche but could also be groundwater. Indeed, the secondary hydroeruptions that took place a year after emplacement of the pyroclastic flows are most likely to be related to seasonal recharge and a rising water table.

6. CONCLUSION

Secondary explosions through pyroclastic flow deposits have occurred in several historical eruptions, indicating they are a common hazard where hot pyroclastic flows are deposited on a wet environment. There has however been relatively little study of the phenomenon, perhaps because the explosion craters and

the associated surge and fallout deposits are readily modified and eroded, and so may often be poorly preserved or not recognized in the geological record.

Our laboratory experiments show that violent outbursts analogous to secondary eruptions can be generated by the drag induced by a distributed flow of gas through a granular material with vertical variations in the minimum fluidisation velocities. Notably, a low-permeability cap is not required to trigger a secondary eruption; in fact, the experiments demonstrate that distributed gas flow up through a granular layer capped with a finer-grained (and so lower permeability) layer made of particles of the same density does not generate jets of particles or craters. However, when the upper layer is coarser, a gas pocket may grow within the finer layer causing the bed to dome upwards until it fails forming a crater and erupting particles. Combining these results with theoretical considerations and constraints from the Mt St Helens 1980 sequence, we conclude that for sufficient steam flux, secondary eruptions can be triggered within pyroclastic flow deposits where there is a fine-grained layer with very low minimum fluidisation velocity under a layer that is coarser and/or contains more dense clasts so that a greater upward velocity of steam is required to fluidise it.

Our experiments with air flow up through layers of unimodal or bimodal glass spheres are very simple; however, the complex behaviour observed provides insights into even more complicated natural secondary eruptions. The experiments are intended only to elucidate the physical origins and triggers of eruptions and not the dynamics of the eruptions themselves, which will be strongly affected by the generation of the steam that drives them. When the eruption is triggered, the associated pressure drop will induce flashing of superheated water at depth

to steam. Steam compressibility may also affect the eruption, which is not the case in the experiments due to the much smaller length-scale and pressure drop. These differences mean that once triggered, the natural secondary eruption is likely to be more energetic than predicted by the processes involved in the experiments.

DATA AVAILABILITY STATEMENT

All datasets generated for this study are included in the article/**Supplementary Material**.

AUTHOR CONTRIBUTIONS

AR conceived the project and supervised AT and SM, who did the experiments and analysis of data. MG re-analyzed and re-plotted the data, and developed some theoretical constraints. MG, AR, and SM created the figures. MG and AR wrote the manuscript. All authors contributed to the article and approved the submitted version.

FUNDING

The research was conducted by the authors in the ordinary course of their employment or education at the University of Bristol. Expenses were paid from academic discretionary accounts.

SUPPLEMENTARY MATERIAL

The Supplementary Material for this article can be found online at: <https://www.frontiersin.org/articles/10.3389/feart.2020.00324/full#supplementary-material>

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Conflict of Interest: The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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